

1 Modeling the Facet Growth Rate Dispersion of β
2 L-Glutamic Acid – Combining Single Crystal Experiments
3 with nD Particle Size Distribution Data

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10 **Abstract**

The growth rate dispersion of needle-like β L-glutamic acid in the length direction is measured using a stagnant solution hot stage microscopy setup. Possible causes of the observed dispersion are analyzed and the resulting distribution of growth rates is used to motivate and reconstruct a distribution of an internal, growth affecting property of the crystals. The latter is then used as the initial condition for a multidimensional, morphological population balance model, whose outputs are fitted to 2D particle size distribution measurements obtained from seeded batch desupersaturation experiments. It is shown, through analysis of both types of data, that a non-zero rate of change in the direction of the new coordinate is required and a phenomenological description of this rate is proposed. The resulting model is able to quantitatively describe experimental data obtained from independent measurement devices, operating at different scales simultaneously.

11 *Keywords:* Crystallization, Crystal Shape, Crystal Growth, Growth Rate Dispersion,
12 Morphological Population Balance Modeling, Hot Stage Microscopy

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Preprint submitted to Chemical Engineering Science

March 27, 2015

13 **1. Introduction**

14 Crystallization is a ubiquitous purification step in the fine chemical and pharmaceu-
15 tical industry. Beside the all-important chemical purity, the distribution of particle
16 sizes and shapes is an important property of the particulate system that determines
17 product quality due to its strong influence on downstream processes. Nevertheless, it
18 is only with recent advancements of imaging tools and computational techniques, that
19 the measurement and modeling of particle size and shape distributions (PSSDs) has be-
20 come more accessible (Wang et al., 2007, 2008; Singh and Ramkrishna, 2013; Schorsch
21 et al., 2012, 2014; Schorsch, 2014), allowing for parameter estimation of face-specific
22 growth rates (Ma and Wang, 2012; Borchert et al., 2014; Oehsenbein et al., 2014) and
23 eventually shape control. The continued progress of these technologies further en-
24 ables gaining unprecedented insight into the mechanisms affecting the size and shape
25 of crystals, thereby creating the possibility of studying crystallization processes on a
26 more fundamental level.

27 An interesting topic of research in which—historically—imaging methods have been of
28 great importance, is that of growth rate dispersion (GRD). Indeed, the discovery and
29 subsequent investigation of the fact that a number of (in)organic crystal systems exhibit
30 large variations of their growth rate has heavily relied on these techniques. Growth rate
31 dispersion may be present both in the temporal domain, i.e., a single crystal’s growth
32 rate may fluctuate over time, as well as within a population of crystals, i.e., crystals
33 exhibit different growth rates when exposed to identical experimental conditions even
34 when they have the same size and shape. While the underlying, physical mechanisms
35 leading to dispersed growth rates are still debated (cf. Section 3.1), the consequence of
36 GRD for crystallization processes is well-known: an otherwise unexpected broadening
37 of the particle size distribution during growth (Wright and White, 1969; Janse and
38 de Jong, 1976; Tavare, 1985).

39 PSSD broadening itself is a phenomenon which is frequently observed experimentally,

40 yet it is often neither modeled quantitatively nor is its exact cause investigated in detail.
41 It is thus likely that in a comparably large number of instances, the effects of growth rate
42 dispersion are falsely attributed to either agglomeration, breakage, spatial variations in
43 the continuous phase within the crystallizer or size dependent growth or vice versa, a
44 fact which has been acknowledged by multiple authors (Garside, 1985; Tavare, 1985;
45 Klug and Pigford, 1989; Ulrich, 1989; Rojkowski, 1993; van Peborgh Gooch et al.,
46 1996; Ma et al., 2002). The role of a correct identification step becomes more apparent
47 given recent efforts in the area of model-based optimization and control of processes
48 (Ma and Wang, 2012; Majumder and Nagy, 2013; Ochsenbein et al., 2013), where
49 model mismatches may lead to unpredicted and undesired behavior of the system when
50 subjected to inputs that have been derived based on an incomplete model.

51 The overwhelming majority of studies that have investigated GRD in depth have tack-
52 led the problem using measurements of facet growth kinetics obtained from a small
53 number of crystals—at a single operating condition—using techniques such as hot stage
54 light microscopy, Michelson interferometry and atomic force microscopy. However,
55 the consequences of the determined extent of GRD for crystal populations are rarely
56 investigated in a quantitative manner. We believe that the combination of different, in-
57 dependent measurement tools, operating at different scales and with different accuracy,
58 presents a promising approach to achieve a quantitative description of GRD at all lev-
59 els. Hence we propose to couple growth measurements of a number of single crystals
60 (size evolution tracked at a single operating condition) with precise measurements of
61 the instantaneous particle size and shape distributions that stem from desupersaturation
62 experiments carried out in a well-mixed batch crystallizer.

63 In particular, we aim at re-evaluating measurements obtained previously, in which
64 PSSD broadening had been provisionally accredited to size dependent growth (Ochsen-
65 bein et al., 2014), in the light of GRD. The resulting model, a multidimensional (mor-
66 phological) population balance equation (nD PBE), represents a reconciled and accu-

67 rate description of the facet growth rate dispersion of β L-glutamic acid (β L-Glu). We
68 emphasize, however, that our intention explicitly is *not* to conclusively determine the
69 physical cause of the observed growth rate dispersion. Rather, we aim at establishing a
70 procedure which uses a more phenomenological (yet quantitative) description of GRD,
71 that remains largely independent of its exact origins, but which eventually may allow
72 to draw some conclusions regarding the possible mechanisms.

73 This work is organized as follows: first, the methods used to obtain experimental data
74 are described in Section 2. Second, in Section 3, the theoretical basis for growth rate
75 dispersion and its description via population balance models are presented together
76 with an outline of the fitting procedure used in this work. The results of the single
77 crystal experiments, the final fitting and a possible interpretation of the results are given
78 in Section 4. In Section 5 the results of this study are discussed before we present
79 conclusions in Section 6.

80 **2. Materials and Methods**

81 *2.1. Materials*

82 L-Glutamic acid monosodium salt hydrate (Sigma Aldrich, Buchs, Switzerland, purity
83 > 99%) and hydrochloric acid (Fluka, Buchs, Switzerland, 37-38%) were used as de-
84 livered. Deionized and filtered (filter size 0.22 μm) water was obtained from a MilliQ
85 Advantage A10 system (Millipore, Zug, Switzerland). L-glutamic acid crystallizes in
86 two known polymorphs, i.e., the metastable α and the stable β polymorph, which are
87 monotropically related (Sakata et al., 1961). Seed crystals of the β polymorph were
88 obtained by allowing crystals of the α polymorph to undergo a solution mediated poly-
89 morph transformation according to the procedure described in Ochsenein et al. (2014).
90 β L-Glu crystals grow in a needle shape whose morphology exhibits three facet fami-
91 lies, namely {010}, {021}, and {101} (Wang et al., 2007). The unit cell parameters are
92 $a = 5.17 \text{ \AA}$, $b = 17.34 \text{ \AA}$, $c = 6.95 \text{ \AA}$ and the space group is $P2_12_12_1$ (Hirokawa, 1955).

93 2.2. 2D PSSD and Concentration Measurement

94 The data used in this work is part of that obtained by Ochsenein et al. (2014). In
95 that work, seeded desupersaturation experiments with varying initial concentrations
96 were performed at constant temperatures in a 2 L temperature controlled stirred tank
97 crystallizer with a stirring rate of 250 rpm. Concentration data was recorded using an
98 ATR-FTIR spectrometer (ReactIR 45m, Mettler Toledo Switzerland) while measure-
99 ments of the 2D PSSD were obtained using a stereoscopic imaging device, presented
100 elsewhere (Schorsch et al., 2014). For the purpose of this paper we selected four ex-
101 periments at 25°C with initial supersaturations of 1.10, 1.15, 1.20 and 1.25 and whose
102 experimental durations typically lie in the order of six to ten hours. A short summary of
103 the PSSD reconstruction procedure is provided in the following: the suspension is sam-
104 pled continuously from the crystallizer and passed through an *ex situ* flow through cell
105 before it is fed back to the system. Particles within the cell are photographed from two
106 orthogonal directions; after a matching and classification step, size and shape are cal-
107 culated automatically. In the case of β L-glutamic acid, each particle is approximated
108 as a cylinder and characterized by its length, L_1 , and width, L_2 . The multidimensional
109 particle size distribution is finally reconstructed using all particles measured within the
110 sampling interval (five minutes) via a binning procedure. The resulting distributions
111 are typically based on several tens of thousands of particles each and allow quantitative
112 analysis of the data (Schorsch et al., 2014; Ochsenein et al., 2014). Note that due to
113 the slow dynamics of the desupersaturation experiments carried out in this work, the
114 time required to obtain a PSSD is negligible.

115 2.3. Hot Stage Setup

116 In order to observe the growth of single crystals in a supersaturated solution a tem-
117 perature controlled measurement cell (diameter: 13 mm, height: 3 mm) made from
118 stainless steel was constructed. The cell and its plastic cover, which prevents evapo-
119 ration of the solvent, are schematically shown in Figure 1. The lower part of the cell

120 is comprised of a custom heat sink that is connected to a Peltier element, allowing for
121 rapid and accurate changes of temperature in the measurement cell. The measurement
122 cell is placed under a Zeiss Axioplan microscope that allows for magnifications from
123 $5\times$ to $20\times$ and captures images automatically with a desired frequency. The experi-
124 mental procedure involves placing a single crystal into the measurement cell, which
125 was filled with saturated solution at a given temperature. The temperature of the solu-
126 tion is then rapidly decreased to the final value, thereby inducing supersaturation and
127 hence crystal growth. An exemplary image of a growing β L-glutamic acid crystal is
128 shown in Figure 2. Analogously to the PSSD measurement, the length L_1 and the width
129 L_2 of the projection are evaluated and their rate of change is used for the determination
130 of growth kinetics. It is worth noting that there is not always a simple one-to-one rela-
131 tionship between the rate of change of L_1 (or L_2) as defined above, and the growth rate
132 of a single crystal facet. Indeed, the measured width of β L-glutamic acid, L_2 , depends
133 not only on the rotation of the needle with respect to the camera, but also on the extent
134 to which two independent facets, i.e., $\{021\}$ and $\{010\}$, have grown. Nevertheless, the
135 measured length of a β L-glutamic acid needle can be shown to be a function solely of
136 one facet type, namely the $\{101\}$ facet (Kitamura and Ishizu, 2000; Ochsenbein et al.,
137 2014). Since the rate of change of L_1 , i.e., G_1 and the growth rate in direction of the
138 $\{101\}$ facet, $G_{\{101\}}$, are proportional, all qualitative statements for the growth rate of
139 measured L_1 are valid also for the true growth rate.

140 Three additional points are worth making: first, since the solution volume is large com-
141 pared to the volume of the crystal, the supersaturation remains virtually constant even
142 when the crystal grows (which can be confirmed by a simple mass balance and was
143 verified experimentally). Second, in the light of the extensive literature concerning ef-
144 fects of strain on crystal growth (see Section 3), it was opted not to fix crystals to the
145 measurement cell, as this might introduce additional strain in the crystal, which in turn
146 could affect the growth rate measurements. Third, this design makes the application

147 of strong convection in the measurement cell impossible, so that our setup is operated
148 under stagnant conditions, as in many other works (Wang and Mersmann, 1992; Jones
149 and Larson, 2000; Virone et al., 2005; Flood, 2010; Dincer et al., 2014; Nguyen et al.,
150 2014). From our previous study on crystals of the β polymorph of L-glutamic acid it
151 is known that growth at low supersaturations is comparably slow (Ochsenbein et al.,
152 2014); an analysis of the characteristic time scales suggests that diffusion is unlikely
153 to limit the crystal growth rate under the given conditions. Furthermore, the crystal
154 growth rates measured for the single crystals compare well with the growth rate esti-
155 mated from whole crystal populations in a stirred vessel, which further supports this
156 conclusion. A more detailed discussion can be found in Section 5.

157 **3. Theory**

158 *3.1. Causes of Growth Rate Dispersion*

159 Janse and de Jong (1976) were probably the first to coin the term “growth rate dis-
160 persion” (GRD) to describe the phenomenon of a spread in growth rates for $K_2Cr_2O_7$
161 crystals; an observation also made prior by Wright and White for sucrose crystals and
162 Natal’ina and Treivus for sucrose and KDP crystals (Wright and White, 1969; Janse
163 and de Jong, 1976; Ulrich, 1989). Soon, it was conjectured that the cause of GRD
164 might be the variation of surface dislocation densities, whose effect on the growth rate
165 is both predicted by Burton-Cabrera-Frank (BCF) theory and confirmed by experimen-
166 tal evidence (cf. Shiau (2003); Dincer et al. (2014) for recent works).

167 These results notwithstanding, a number of additional factors influencing the growth
168 of crystals have been identified. These include effects caused by lattice strain (Bhat
169 et al., 1987; Ristić et al., 1988; van der Heijden and van der Eerden, 1992; Zacher
170 and Mersmann, 1995; Herden and Lacmann, 1997; Sherwood and Ristić, 2001), or
171 surface roughening (Pantaraks and Flood, 2005; Flood, 2010). These phenomena can
172 cause a fluctuation of the observed growth rate (variability over time) and a growth rate

173 variance in a population of crystals even when the crystals seem macroscopically iden-
174 tical and the operating conditions (e.g., supersaturation, temperature, etc.) are constant
175 and the same for all crystals. In contrast, Singh and Ramkrishna (2014) explained time-
176 varying growth rates by microscopic supersaturation fluctuations, which, assuming that
177 a crystallizer is well-mixed, cannot explain different growth rates for macroscopically
178 identical crystals.

179 Given the ongoing debate on the subject, it seems reasonable to assume that growth rate
180 dispersion in general is caused by the interplay of various mechanisms, whose relative
181 importance is likely co-determined by the crystalline system itself, the instantaneous
182 operating conditions and the particle history (Finnie et al., 1999; Jones et al., 2000;
183 Jones and Larson, 2000; Sherwood and Ristić, 2001; Pantarakis and Flood, 2005).

184 From a descriptive point of view, two models of growth rate dispersion under the con-
185 ditions typically found in growth experiments (carried out at constant supersaturation
186 and temperature) have emerged: the random fluctuations (RF) and the constant crystal
187 growth (CCG) model. While in the former case, GRD is modeled as temporal varia-
188 tions of the growth rate around a given (but constant) expected value, which gives rise
189 to a second-order dispersive term in the population balance equation, the latter model
190 assumes that crystals are intrinsically born with a distribution of growth rates. While
191 the RF and the CCG models are not mutually exclusive, combined approaches are rare
192 (Zumstein and Rousseau, 1987a,b) and purely CCG-like interpretations are more fre-
193 quently found in literature. Consequently, a large number of researchers fit standard
194 probability functions, such as normal, log-normal or gamma distributions to time aver-
195 aged growth rates obtained from single crystal experiments (Garside and Ristić, 1983;
196 Wang and Mersmann, 1992; Zikic et al., 1996; Finnie et al., 1999; Mitrović et al., 2002;
197 Flood, 2010).

198 In this work, a CCG-like approach is used as well, as it matches the experimental
199 observations presented in Section 4.1; however, the growth rates themselves are not

200 assumed to be distributed properties as done elsewhere (e.g., by Janse and de Jong
 201 (1976); Zumstein and Rousseau (1987a,b)). Rather, a lumped quantity, referred to
 202 as *growth affecting property (gap)*, will be taken as the single factor modifying the
 203 growth rates of a crystal (see Section 3.3), an approach that is structurally similar to
 204 that of Gerstlauer et al. (2001) (cf. Table 1 for a more detailed comparison). Given
 205 the complexity of GRD mechanisms and in the absence of any obvious *a priori* choice
 206 for the dominating cause of growth rate dispersion in the β L-glutamic acid system, the
 207 introduction of this proxy variable allows for a considerable degree of flexibility while
 208 maintaining a manageable level of model complexity.

209 3.2. Population Balance Modeling

210 A large number of crystallization processes can be described using the deterministic
 211 population balance framework (Hulburt and Katz, 1964; Ramkrishna and Singh, 2014),
 212 including those with considerable growth rate dispersion. An overview of a selection
 213 of works modeling GRD is given in Table 1. A general formulation for a well-mixed
 214 batch system with continuous internal coordinates is given by

$$\frac{\partial}{\partial t} f(t, \mathbf{x}) + \nabla_{\mathbf{x}} \cdot [\mathbf{G}(t, \mathbf{x}, \mathbf{z}) f(t, \mathbf{x})] = B(t, \mathbf{x}, \mathbf{z}) - D(t, \mathbf{x}, \mathbf{z}) \quad (1)$$

215 where f is the number density function describing the particulate population, which is
 216 defined over the set of internal coordinates \mathbf{x} , and \mathbf{G} is the velocity field describing the
 217 rate of change of internal coordinates, which is usually a function of the state of the
 218 continuous phase \mathbf{z} (supersaturation, temperature, pH, etc.) as well. B and D represent
 219 “birth” and “death” terms, respectively, allowing for the incorporation of additional
 220 mechanisms such as nucleation, agglomeration or breakage of particles. In the case of
 221 β L-Glu, whose needle-like crystal shape is approximated by a cylinder with length L_1
 222 and width L_2 and which at the conditions considered does only exhibit growth, Eq. (1)
 223 can be recast as

$$\frac{\partial f}{\partial t} + \frac{\partial (G_1 f)}{\partial L_1} + \frac{\partial (G_2 f)}{\partial L_2} + \frac{\partial (G_w f)}{\partial w} = 0, \quad (2)$$

224 where we have made use of the surrogate *gap* variable w that was introduced earlier.
 225 Note that the applicability of the assumption of absence of nucleation, agglomeration
 226 and breakage was verified earlier by Ochsenein et al. (2014).

227 While it is clear that the growth rates (in the isothermal case) are generally given as
 228 $G_i = G_i(S, \mathbf{L}, w)$ with $i \in \{1, 2\}$, i.e., they are defined as functions of the supersaturation
 229 S , the size vector \mathbf{L} , and the *growth affecting property* w , their exact functional form
 230 is not obvious and depends largely on the nature of w . Similarly, the last term on the
 231 l.h.s. of Eq. (2) describes the evolution of the population along the *gap* coordinate; a
 232 suitable choice for $G_w = dw/dt$ is also not evident. A set of meaningful options for all
 233 convective terms based on fundamental considerations will be presented and discussed
 234 in Section 3.3.

235 Furthermore, the supersaturation in this work is defined as

$$S = \frac{c}{c^*(T)} \quad (3)$$

236 where c is the solute concentration in the liquid phase and $c^*(T)$ is the solubility and
 237 the initial and boundary conditions for the PBE are written as

$$f(0, \mathbf{L}, w) = f_0(\mathbf{L}, w) \quad (4)$$

$$f(t, 0) = 0 \quad (5)$$

238 where $f_0(\mathbf{L}, w)$ is the size and *gap* distribution of the seed particles, the derivation
 239 of which is outlined in Section 3.4. From f , different marginal distributions can be

240 reconstructed, such as the particle size and shape distribution f_s , which is given by

$$f_s(t, \mathbf{L}) = \int_0^\infty f(t, \mathbf{L}, w) dw \quad (6)$$

241 f_s can be measured by imaging devices such as the one presented by Schorsch et al.
 242 (2014). To satisfy the conservation of mass, a mass balance equation for the solute
 243 concentration in the liquid phase is needed. A general formulation for a closed system
 244 is given by

$$\frac{dc}{dt} = -\rho_c \frac{d}{dt} \int_C V_c(\mathbf{L}) f_s(t, \mathbf{L}) d\mathbf{L} \quad (7)$$

245 where C is the size domain, ρ_c is the density of the crystalline phase and $V_c(\mathbf{L})$ is
 246 the volume of the crystal with characteristic sizes \mathbf{L} . In particular, for the cylindrical
 247 particles considered here, $V_c(L_1, L_2) = \frac{\pi}{4} L_1 L_2^2$, $C = \mathbb{R}^2$, and Eq. (7) can be expressed
 248 as:

$$\frac{dc}{dt} = -\rho_c \frac{\pi}{4} \frac{d\mu_{12}}{dt} \quad (8)$$

249 where μ_{12} is a cross-moment of $f_s(t, L_1, L_2)$, in general defined as

$$\mu_{ij} = \int_0^\infty \int_0^\infty L_1^i L_2^j f_s(t, L_1, L_2) dL_1 dL_2 \quad (9)$$

250 The initial condition for Eq. (7) is:

$$c(0) = c_0 \quad (10)$$

251 with c_0 being the initial solute concentration.

252 The three dimensional, first order partial differential equation in Eq. (2), together with
 253 the material balance Eq. (8) is solved similar to a standard morphological PBE with
 254 three internal coordinates, using a customized finite volume *high resolution* method
 255 which solves the corresponding equations for the bounding box containing the distri-

256 bution (Leveque, 2002; Gunawan et al., 2004; Ochsenein et al., 2014). This method
 257 permits the full reconstruction of the distribution at all times with reasonable computa-
 258 tional effort and thus enables a comparison between measured and simulated PSSDs.

259 3.3. Convective Terms

260 In the following, a brief discussion of the various convective terms in Eq. (2) is pro-
 261 vided. We will begin with an examination of the size growth rates G_1 and G_2 and the
 262 possible impact of w on those rates followed by an analysis of G_w .

263 3.3.1. Size Growth Rates

264 Under the conditions encountered in this work and up to even higher supersaturations,
 265 the growth of β L-Glu was found to be surface integration limited and could be well-
 266 described by a “Birth and Spread” type description (Kitamura and Ishizu, 2000; Cornel
 267 et al., 2009; Ochsenein et al., 2014). These results notwithstanding, a useful and
 268 flexible empirical relationship for supersaturation dependent growth rates at constant
 269 temperature is given by

$$G_i^0(S) = p_{i,1} (S - 1)^{p_{i,2}} \quad i \in \{1, 2\} \quad (11)$$

270 where $p_{i,1}$ and $p_{i,2}$ are parameters. The simplest possible approach to incorporate the
 271 effect of a *growth affecting property* is by assuming that the growth rates are simply
 272 multiplied by some constant, supersaturation and temperature independent factor w

$$G_i(S, w) = w p_{i,1}^0 (S - 1)^{p_{i,2}} \quad i \in \{1, 2\} \quad (12)$$

273 This result is also obtained when GRD is qualitatively explained through BCF theory,
 274 i.e., by variations of the number of co-operating spirals (Garside and Davey, 1980; Klug
 275 and Pigford, 1989; Bohlin and Rasmuson, 1992; Shiau, 2003). Note that in Eq. (12),
 276 we set $p_{i,1}^0 = 1 \text{ m s}^{-1}$ as w and $p_{i,1}$ cannot be decoupled.

277 Another common assumption stems from investigations of strain effects, and relates
 278 growth rate changes to variations of the chemical potential of the crystals, or in other
 279 words, their solubility. The effective solubility thus becomes (Bhat et al., 1987; van der
 280 Heijden and van der Eerden, 1992; Gerstlauer et al., 2001; Jones et al., 2000; Virone
 281 et al., 2005)

$$c_{\text{eff}}^*(T, w_s) = c^*(T) \exp\left(\frac{w_s}{RT}\right) \quad (13)$$

282 where w_s is the molar strain energy and the growth rate is given accordingly by

$$G_i(S, w_s) = p_{i,1} \left(S \exp\left(-\frac{w_s}{RT}\right) - 1 \right)^{p_{i,2}} \quad i \in \{1, 2\} \quad (14)$$

283 Since we are more interested in the functional form of Eq. (14) than its physical in-
 284 terpretation and as we operate at a single temperature, we will use the substitution
 285 $w = w_s/RT$ in our fittings that employ such a model, i.e., in these cases G_i is written as

$$G_i(S, w) = p_{i,1} (S \exp(-w) - 1)^{p_{i,2}} \quad i \in \{1, 2\} \quad (15)$$

286 It should be noted that Eq. (15) may result in negative growth rates for crystals ex-
 287 hibiting considerable strain, i.e., if $w_s > RT \ln(S)$. While the existence of such highly
 288 strained crystals cannot be ruled out, we never observed shrinkage (dissolution) of
 289 crystals in our experiments. In this work, all growth rates are hence constrained to be
 290 non-negative.

291 An examination of the two models reveals that they predict a different behavior of the
 292 growth rate distribution at different supersaturations: Eq. (12) assumes a constant, su-
 293 persaturation independent distribution of growth rates whereas Eq. (15) implies distri-
 294 butions which are strongly affected by varying supersaturation. Experimental evidence
 295 of both behaviors exists, though an increase of growth rate dispersion for increasing

296 supersaturations is reported more often (Finnie et al., 1999; Jones et al., 2000; Flood,
297 2010). We will refer to approaches corresponding to Eq. (12) and Eq. (15) as the BCF-
298 and the strain-type of growth, respectively, and will try to fit our data using either op-
299 tion individually. Whereas it is conceivable to apply a growth rate that incorporates
300 both approaches simultaneously (Jones and Larson, 2000), we will assume that the
301 true effect of the *growth affecting property* w is dominated by one type or the other.
302 We conclude this section with a final remark. There is reason to believe that different
303 facets may be affected differently by the *growth affecting property*, an effect that was
304 also observed experimentally (Sherwood and Ristić, 2001). However, such a situation
305 can only be reliably detected experimentally when the growth rates of various facets
306 are large or the measurement interval is sufficiently long. In order to model growth rate
307 dispersion in a new direction, in principle, either an additional *gap* coordinate needs to
308 be introduced or a (different) relationship between the *growth affecting property* and
309 the new direction needs to be established. In this work, it will be assumed that the
310 effect of the *gap* on the growth rates is either exactly identical for both facets or that
311 w does not affect the growth rate in the width direction; all fittings were performed
312 making either assumption.

313 3.3.2. *gap* Rate of Change

314 An important—though often neglected—question in the area of growth rate dispersion is
315 that of whether the growth rate of a single crystal, growing under constant experimental
316 conditions, will remain constant over long time spans (Mitrović et al., 2008, 2009) and
317 related to this, whether or not the growth rate distribution in the reactor is stationary.
318 From a modeling perspective, this determines the nature of the *gap* rate of change,
319 which in our case takes on the unit s^{-1} . Clearly, a physical approach would require a
320 sound understanding of the exact nature of the *growth affecting property* in question.
321 Unfortunately, little is known regarding the evolution of these properties beyond some
322 qualitative speculation.

323 In many classic CCG approaches, which typically employ a BCF type modification
324 to the growth rates, G_w is assumed to be zero (cf. Table 1). In models employing
325 strain-type growth rates, G_w is often predicted to be negative (strain decreases over
326 time; growth rate increases) and Gerstlauer et al. (2001) give an overview of various
327 possible strain “relaxation” rates based on different assumptions of the absolute lattice
328 strain of crystals and its dependence on the crystal size. In other studies, a temporary
329 decrease of the growth rate after periods of fast growth is reported for crystals subjected
330 to supersaturation swings (Pantaraks and Flood, 2005; Flood, 2010). Table 1 contains
331 information regarding the different assumptions about the rates made in other modeling
332 works. In this work, we will set out to determine whether or not a static *gap* distribu-
333 tion is able to describe the experimental data and, if not, to deduce a number of key
334 characteristics of a non-zero G_w by considering various models for G_w and evaluating
335 their goodness of fit with our experimental data. In this context, we highlight the fact
336 that, in the absence of any experimentally verified and quantitative description of the
337 *gap* rate of change, we utilize a completely empirical expression for G_w .

338 3.4. Fitting Procedure

339 A key objective of this work is the quantitative description of growth rate dispersion,
340 both for individual crystal experiments and for experiments with populations of crystals
341 within an agitated batch crystallizer. The demonstration of the feasibility of a simulta-
342 neous description is necessary (though not sufficient) to prove the relevance of single
343 crystal data for the behavior of real vessels, yet it is rarely shown (Klug and Pigford,
344 1989).

345 Two types of fitting procedures are applied in this work, both of which are designed to
346 solve the problem of the unknown initial distribution of the *growth affecting property*
347 while establishing a connection between single crystal and population data. For both
348 approaches, however, it is assumed that the distribution of growth rates and thus of the
349 *gap* is independent of the initial size and shape of crystals (Zumstein and Rousseau,

1987a), an assumption whose validity will be checked in Section 4.1. The independence assumption implies that

$$f(\mathbf{0}, \mathbf{L}, w) = f_s(\mathbf{0}, \mathbf{L}) P_w(\mathbf{0}, w) \quad (16)$$

where P_w is the *gap* probability density distribution. The two procedures, both visually summarized in form of a flowchart in Figure 3, differ in the way that P_w is estimated. In the first case, P_w is assumed to be a normal distribution, whose two parameters are fitted along with the remaining growth parameters (‘no’ case in Figure 3). Clearly, in this way, the observed distribution of growth rates from the single crystal experiments is not necessarily recovered, yet two additional degrees of freedom (mean and variance of the Gaussian) are gained for the fitting. In contrast, in the second approach (‘yes’ scenario in Figure 3), the single crystal data is fitted well by construction. This is achieved by fitting the parameters of the normal *gap* distribution in a separate step before the actual start of the simulation. In particular, those parameters are found by separately fitting a normal distribution to the dataset $\tilde{\mathbf{w}}$, originating from the single crystal experiments, defined as

$$\tilde{\mathbf{w}} = \begin{bmatrix} \tilde{w}^{(1)} \\ \tilde{w}^{(2)} \\ \vdots \\ \tilde{w}^{(101)} \end{bmatrix} = \begin{bmatrix} g(\tilde{G}_1^{(1)}) \\ g(\tilde{G}_1^{(2)}) \\ \vdots \\ g(\tilde{G}_1^{(101)}) \end{bmatrix} \quad (17)$$

where $\tilde{G}_1^{(i)}$ is the observed growth rate for the i -th single crystal and $g(\cdot)$ is the inverse function of $G_1(S = 1.2, w; \mathbf{p})$ given at $S = 1.20$ (i.e., the supersaturation in those experiments) and the current parameter estimate. Note that the exact $g(\cdot)$ depends on the G_1 -function chosen for the fit (either Eq. (12) or Eq. (15)). In the cases in which the inverse element does not exist (Eq. (15) is not bijective), the algorithm chooses the value of w that yields the closest result.

370 Regardless of the choice of fitting, the population balance model is subsequently solved
 371 and its outputs compared to the results of seeded batch desupersaturation experiments,
 372 applying the same methods reported in Ochsenein et al. (2014). In particular, the
 373 maximum likelihood estimate is obtained by minimizing the objective function (Bard,
 374 1974)

$$\Phi(\mathbf{p}) = \frac{N_t}{2} \sum_{i=1}^{N_v} \ln \left[\sum_{j=1}^{N_t} (y_{ij} - \hat{y}_{ij}(\mathbf{p}))^2 \right] \quad (18)$$

375 where N_t is the number of observations, N_v is the number of measured outputs, y_{ij} is
 376 output i at time j and $\hat{y}_{ij}(\mathbf{p})$ is the corresponding model estimate as a function of the
 377 parameters \mathbf{p} . The output vector \mathbf{y}_j at time t_j is given by:

$$\mathbf{y}_j = \begin{bmatrix} c \\ \bar{L}_1 \\ \sigma_{11} \end{bmatrix}_{t=t_j} = \begin{bmatrix} c \\ \mu_{10}/\mu_{00} \\ \sqrt{\mu_{20}/\mu_{00} - (\mu_{10}/\mu_{00})^2} \end{bmatrix}_{t=t_j} \quad (19)$$

378 where \bar{L}_1 is the mean length of the crystals in the PSSD and σ_{11} represents the standard
 379 deviation of the PSSD in L_1 direction.

380 4. Results

381 In this section, results of both the single crystal experiments and the fittings of ensemble
 382 data in an agitated batch crystallizer using various models are provided. First, the
 383 experimental results of the single crystal study are given in Section 4.1. Note that only
 384 an analysis of G_1 is provided, as the growth rate in L_2 direction, i.e., the change in
 385 the width of the crystals, is excruciatingly slow and therefore hard to quantify. The
 386 observed significant dispersion of growth rates in L_1 direction, however, is taken in
 387 Section 4.2 as motivation for the use of GRD models in the fitting of ensemble data
 388 derived from batch desupersaturation experiments conducted at the same temperature

389 (Ochsenbein et al., 2014). The findings of the n D PSD data fitting are divided into two
390 parts, representing the different assumptions made.

391 *4.1. Single Crystal Experiments*

392 The evolution of crystal length over time for a number of crystals during the course of
393 single crystal experiments is shown in Figure 4 where the change in time of L_1 -size
394 with respect to the initial value is plotted. The growth rate G_1 is initially different for
395 different crystals, exhibiting rather large variability around an average value. As time
396 goes by, growth slows down for all crystals and the variability seems to decrease. While
397 some level of fluctuation of the growth rates lying below the precision of the measure-
398 ment cannot be ruled out, it is clear that large, time-independent variations exist among
399 the different crystals. Given the line of reasoning in Section 3.4, the properties of the
400 seed crystals at time $t = 0$ are of particular interest; it was therefore decided to utilize
401 only the first 60 minutes of the single crystal experiments, a period in which the growth
402 rate can be reasonably well approximated as constant.

403 The results of this analysis for 101 particles are visualized in Figure 5, where the scat-
404 ter plot of G_1 as a function of the initial crystal size together with the corresponding
405 histogram are reported. Visual inspection of the data appears to reveal a lack of size
406 dependence of G_1 with regard to the crystal length, L_1 , and only a small effect of the
407 width L_2 . A quantitative assessment of potential size dependence can be performed by
408 means of nonlinear regression, in which the data set is fitted to, e.g.

$$G_1 = k_1(1 + L_1)^{k_2} (1 + L_2)^{k_3} \quad (20)$$

409 The result of said fitting is given in Table 2, where the estimated parameter values,
410 the t -statistics and the corresponding p -values are reported. In this table, the p -values
411 for k_2 and k_3 are of interest. The high p -value obtained for k_2 ($p = 0.54$) indicates
412 that the null hypothesis (the data can be explained by a model with $k_2 = 0$; there is
413 no L_1 dependence) cannot be rejected. However, the same statement cannot be made

414 for L_2 : the p -value of parameter k_3 indicates that the null hypothesis can be rejected
415 with high probability and a size dependence of G_1 on L_2 is therefore probable. The
416 magnitude of the estimated size dependence ($k_3 = 0.32$) can be compared to that of the
417 BL2E model presented in Ochsenein et al. (2014), which was found to be 2.55 ± 0.04 .
418 Both the magnitude of the exponent and the sign of the derivative of G_1 with respect
419 to L_2 highlight that the true effect of size on the growth rate is marginal and cannot
420 explain the observed PSSD broadening in itself. Furthermore, given the bigger relative
421 measurement error in the width direction and the still largely unexplained variance in
422 the data (coefficient of determination $r^2 = 0.2$), the assumption that the distribution
423 of growth rates is independent of the size distribution seems to be in fact a reasonable
424 approximation of the initial condition.

425 We emphasize that the above findings do not necessarily rule out the possibility of
426 having growth rates that are influenced by the initial fragment size of crystals born
427 via secondary nucleation (Wang and Mersmann, 1992; Zekic and Mitrović, 1996), a
428 mechanism potentially important for β L-Glu (Cornel et al., 2009). However, the above
429 results suggest that, for the crystal population present at the beginning of our experi-
430 ments, i.e., for the seed crystals, this effect would have become negligible.

431 4.2. *Fitting Ensemble Data*

432 The results of fitting the ensemble data with the presented *gap* model and increasingly
433 complex convective terms are reported here. It should be noted that the presented fits
434 can be considered optimal neither in the sense of physical accuracy (as the descrip-
435 tions of all rates are merely empirical and cannot reasonably cover all possibilities)
436 nor mathematically (since a guarantee of optimality can generally not be provided for
437 these types of systems), therefore we cannot expect to conclusively validate any one
438 model and final parameters should be interpreted as purely empirical. It is worth not-
439 ing that our optimization routines did repeatedly converge to the same solutions also
440 when started from different initial guesses of the parameters. Regardless, we construct

441 our argument based on the logic that the minimally complex description that is able to
 442 explain the data satisfactorily is likely to possess a set of key features that are present
 443 in the real system and we aim at finding such a model.

444 4.2.1. Static gap Model

445 As has been pointed out, the presence of a distribution of growth rates (caused by
 446 some *gap*) invariably leads to a broadening of the PSSD in the direction of the cor-
 447 responding characteristic size. Furthermore, the rate of PSSD broadening ($d\sigma_{11}/dt$ in
 448 the case of the length direction) is higher when the the underlying *gap* distribution is
 449 wider. The simplest possible assumption for the *gap* content of crystal is that it remains
 450 constant over time, implying a zero rate of change G_w . As pointed out by Gerstlauer
 451 et al. (2001), the resulting model is essentially identical to the constant crystal growth
 452 model, described for example by Zumstein and Rousseau (1987a,b), yet in our case it
 453 is extended to account for particles with two characteristic lengths.

454 We attempted fitting the morphological PBE model using either BCF- or strain-type
 455 growth rates and with or without w dependence of the width growth rate G_2 (i.e., four
 456 different combinations). From these static *gap* models, the best BCF-type fit, repre-
 457 sentative for all results with static *gap*-distributions, was obtained with the following
 458 growth rates

$$G_1(S, w) = wp_{i,1}^1(S - 1)^{4.3} \quad [\text{m s}^{-1}] \quad (21a)$$

$$G_2(S) = 1.3 \times 10^{-2}(S - 1)^{10.0} \quad [\text{m s}^{-1}] \quad (21b)$$

$$G_w = 0 \quad [\text{s}^{-1}] \quad (21c)$$

459 and the resulting fit is illustrated in Figure 6. Furthermore, in Table 3, we report the
 460 mean relative errors (*MRE*) of all quantities, defined for quantity i in a given experi-
 461 ment as

$$MRE_i = \left| \frac{1}{N_t} \sum_{j=1}^{N_t} \frac{y_{ij} - \hat{y}_{ij}}{y_{ij}} \right| \quad (22)$$

462 Clearly, the model is incapable of describing the population data in an adequate manner,
 463 whereas the single crystal data is fitted well by construction, cf. Figure 6(a). In fact, a
 464 reasonable fit of σ_{11} (third row of Figure 6(b)) must be accompanied by a large increase
 465 of the average size of particles, whose magnitude is far greater than that observed
 466 experimentally (second row of Figure 6(b)).
 467 Unsurprisingly, the above result can be improved by fitting the initial *gap* distribution
 468 using a normal distribution, i.e., by adding two additional parameters to each of the four
 469 model variants mentioned above. In that case, the best fit was obtained using a strain-
 470 type growth rate in the length direction and no w dependence in the width growth rate;
 471 resulting in the following growth rate expressions

$$G_1(S, w) = 6.6 \times 10^{-7} (S \exp(-w) - 1)^{1.5} \quad [\text{ms}^{-1}] \quad (23a)$$

$$G_2(S) = 4.8 \times 10^{-5} (S - 1)^{5.9} \quad [\text{ms}^{-1}] \quad (23b)$$

$$G_w = 0 \quad [\text{s}^{-1}] \quad (23c)$$

472 and a fitted initial *gap* distribution with a mean of 0.22 and standard deviation of 0.07.
 473 Such a model allows to reduce the objective function value significantly, as can also be
 474 seen from the overall much better fit in Figure 7(b) and the corresponding entry in Ta-
 475 ble 3. However, this appreciable improvement in the description of the population data
 476 requires a large modification of the initial *gap* distribution, resulting in a growth rate
 477 distribution that is entirely inconsistent with the data obtained from the single crystal
 478 experiments (cf. Figure 7(a)). In particular, in order to describe the PSSD data, from a
 479 modeling point of view, a strong increase of the *gap* distribution variance is required.
 480 This implies the existence a large number of particles whose growth is completely ar-
 481 rested from the beginning of each experiment, an effect that reduces the increase in

482 average size \bar{L}_1 necessary to achieve a given gain in σ_{11} .
483 Summarizing, it was found that describing the two data sets in any satisfactory manner
484 when using a *gap* rate of change of zero ($G_w = 0$) is impossible. While an accurate
485 description of only the PSSD data alone is feasible, this requires the conjuring of a
486 large number of non-growing crystals in the model. Such crystals were however not
487 observed in the single crystal experiments. Moreover, any static model will predict
488 a constant growth rate for each crystal, which markedly contradicts the time resolved
489 ΔL_1 vs. t curves obtained from the single crystal experiments (cf. Figure 4).

490 4.2.2. *Dynamic gap Model*

491 As discussed in Section 3.3.2, considering the possible physical causes that motivated
492 the introduction of the *growth affecting property* variable w in Section 3.1 it is not
493 unreasonable to assume that the absolute or relative content of the intrinsic property
494 might be subject to changes over time, i.e., that $G_w \neq 0$. The single crystal experiments
495 results (cf. Figure 4), too, seem to indicate a change of the growth rate over time. While
496 the information of the change in G_1 contained in these experiments could not be utilized
497 in a quantitative manner (see Section 5.1 for details), these experiments allow us to
498 surmise two important qualities of the dynamic behavior of the GRD. First, it allows
499 us to infer the sign of G_w (namely, G_w is negative when using a BCF-type modification
500 of G_i and positive in the strain-type case; the rate of growth slows down). Second, it
501 can be seen that the variance of the G_1 (and hence also the *gap*) distribution decreases
502 with time, which remains true regardless of the growth rate modification used.

503 The latter observation is of particular importance given the results with the static *gap*
504 model in Section 4.2.1, where it evident that the quality of fit for the batch data im-
505 proves with increasingly broad (static) *gap* distributions, yet that such distributions
506 differ significantly from the experimentally observed ones. Clearly, a mere decrease of
507 the growth rate—when applied to all crystal sizes uniformly— is therefore also not able
508 to describe the batch experiments.

509 In order to reconcile the above considerations, we propose the presence of a selective
510 driving force that makes a certain type of crystals change their growth rate faster or
511 slower than others. One of the ways to achieve a significant increase in the width of the
512 PSSD in L_1 direction, σ_{11} , early on, is to make this driving force depend on the size of
513 the crystal. We therefore suggest the following empirical expression for the *gap* rate of
514 change, G_w

$$G_w = p_{w,1} L_1^{p_{w,2}} G_1^{p_{w,3}} \quad (24)$$

515 From the above mentioned models (employing the four different combinations of growth
516 rates) with this dynamic *gap* rate of change the following model yielded the best fit we
517 could identify

$$G_1(S, w) = 2.0 \times 10^{-6} (S \exp(-w) - 1)^{2.2} \quad [\text{m s}^{-1}] \quad (25a)$$

$$G_2(S, w) = 3.6 \times 10^{-4} (S \exp(-w) - 1)^{4.5} \quad [\text{m s}^{-1}] \quad (25b)$$

$$G_w = 36.8 L_1^{-2.0} G_1^{1.2} \quad [\text{s}^{-1}] \quad (25c)$$

518 The fitting results are illustrated in Figure 8 and Table 3, where a clear improvement of
519 the quality of fit is visible. Nevertheless, there still exists a non-negligible discrepancy
520 between experimental results and model output, which might be caused by a (still) too
521 simplistic model of G_w . Moreover, while multiple initial points were evaluated in the
522 parameter space and different optimization algorithms were used, the identification of
523 global optima is a difficult endeavor for these complex models.

524 In addition to showing fitting outputs, analyses of the different marginal distributions
525 are possible. In Figure 9, various volume weighted, marginal distributions, (defined
526 in a similar manner as the size and shape distribution in Eq. (6)) for one experiment
527 ($S_0 = 1.20$) in the beginning and end are shown; in the case of the PSSD, the model out-
528 put is compared with the experimentally measured distributions. Focusing first on the

529 final PSSD (Figure 9(d)), one can see that the variance of the model output is slightly
530 too low, but that the overall movement of the PSSD is generally well captured. As
531 shown in the remaining marginal distributions, i.e. figures c) to f), there is a significant
532 torsion of the distribution. In the end of the process, larger crystals generally possess a
533 smaller *gap* content due to the fact that a) crystals with low *gap* content grow faster (in
534 the case of strain-type growth) and b) smaller crystals have a faster build-up of *gap* (cf.
535 Eq. (25c)). Furthermore, in Figure 10, the initial/final *gap* and growth rate distribution
536 for the same operating conditions are shown, thus indicating that the growth rate dis-
537 tribution is indeed expected to decrease both in mean and variance over the course of
538 the process, a behavior not unlike that exhibited in the single crystal experiments (cf.
539 Figure 4).

540 In addition, we have tested the predictive capabilities of the dynamic *gap* model by
541 means of two types of comparisons, the results for which we report in Table 3. First,
542 the ability to interpolate was verified by fitting three out of the four experiments at $T =$
543 25°C and predicting a fourth, whose initial supersaturation lies in between the others.
544 Second, we have compared the model prediction with the parameters in Eq. (25) to an
545 additional experiment performed in our initial study, conducted at a higher temperature
546 (30°C) and with a supersaturation of 1.18 (labeled VER1 in (Ochsenbein et al., 2014)),
547 i.e., in this case we use the model to extrapolate in terms of temperature. In both cases,
548 the predictive capabilities of the model are satisfactory, as indicated by the small mean
549 relative errors in Table 3, with a clear decrease in accuracy for the latter case, in which
550 the model is extrapolated.

551 In order to arrive at a definitive picture of the physical mechanism(s) underlying growth
552 rate dispersion, a substantially extended experimental data set, consisting of experi-
553 ments conducted in realistic batch conditions as well as experiments probing the fun-
554 damental origin of the growth affecting property would be required (see also the dis-
555 cussion in Section 5). Nevertheless, a *preliminary* interpretation, consistent with the

556 experimental evidence as well as with the proof-of-concept fitting results provided in
557 this article, shall be given. A valid hypothesis might be that the surface of the seed
558 crystals is initially rough, i.e., riddled with kink sites, leading to an acceleration of
559 growth in the early stages. With time, the particles might slowly undergo a healing or
560 refacetting step, whose duration and extent might be affected by the crystal size (e.g.,
561 via the total crystal surface area).

562 **5. Discussion**

563 *5.1. Single Crystal Data*

564 As one of the major goals of the current work is to establish a quantitative connection
565 between shape measurements conducted at the single particle and at the population
566 level, a discussion of the suitability of the used hot stage setup and the corresponding
567 single crystal data is essential. It is clear that, for any comparison to be meaningful,
568 the growth conditions in the lab-scale reactor and the hot stage should be compara-
569 ble. It is well-known that impurities in the crystals or in the solution could change the
570 growth rate (Sangwal, 2007; Vetter, 2012). However, all solutions and seed crystals
571 used in this work stem from the same batch of L-glutamic acid (which was also used
572 to generate the population data reported in Ochsenbein et al. (2014)) and have been
573 carried out using highly pure water as solvent. Therefore, the GRD observed in our
574 experiments cannot simply be explained by varying impurity profiles between different
575 experiments. However, we can immediately identify two important aspects that are
576 absent in the hot stage: stirring and particle collisions. Concerning the first point, it
577 has already been pointed out that the growth of β L-glutamic acid is slow enough to be
578 surface-integration controlled even in the absence of stirring. Regarding the missing
579 particle-particle (or particle-impeller/particle-wall) interactions: the growth rate dis-
580 tribution might well be affected by collisions, e.g., by causing imperfections in the
581 growing crystal surfaces. It seems reasonable to assume that collisions, due to their in-

582 herently stochastic nature, would therefore intensify an inherently present growth rate
583 distribution. However, by additionally trying to fit the *gap* distribution in Section 4.2.1,
584 we have implicitly accounted for the possibility of a broader distribution. Regardless,
585 we believe that solely relying on single crystal experiments to characterize the extent
586 of GRD in an industrial crystallization process is not advisable.

587 Finally, we would like to comment on the possibility of extracting information regard-
588 ing G_w (and its potential size dependence) from single crystal data. While potentially
589 feasible, a quantitative analysis would require a large number ($\gg 100$) of sampled crys-
590 tals, whose initial size and shape should ideally be controlled, a feat that is difficult
591 to achieve. While such measurements would be of great interest, we regard them as
592 beyond the scope of the current work.

583 5.2. Modeling and Fitting

584 The modeling and fitting procedures presented here are the key tools allowing for a
585 better interpretation of the experimental data. It is therefore important to clearly outline
586 the possible applications together with the limitations of the described morphological
587 population balance equations.

588 We emphasize the fact that an important assumption made is that of a size independent,
589 initial growth rate distribution. While the experimental evidence reported in Section 4.1
600 suggests that this approximation is a meaningful one, it is worthwhile to discuss the
601 potential ramifications of it being incorrect. Essentially, the necessity for G_w to be a
602 function of size diminishes with increasing violation of the above assumption. Hence,
603 without a more detailed analysis of the size dependence of the growth rate dispersion
604 of the seed crystals, involving again the measurement of many more particles, we can-
605 not necessarily rule out the possibility that the proposed size dependence of G_w is an
606 artifact of some underlying effects and care should be taken not to over-interpret the
607 results. Nonetheless, it should be noted that the dynamic *gap* model presented in Sec-
608 tion 4.2.2 neither represents just an increase in the number of parameters in order to

609 fit more data better, nor does it serve as a simple shift of the size dependence from the
610 growth rate G_1 to some other convective term. The lack of a strong size dependence
611 of the growth rate together with the large observed scatter does *necessitate* the use of
612 (at least) one additional internal coordinate to achieve a more physically correct model.
613 The size and shape of crystals or the properties of the continuous phase, which are the
614 only physical variables in the classic population balance model without growth rate
615 dispersion, are demonstrably insufficient to explain both types of experimental obser-
616 vations reported here. Furthermore, the fact that a size dependent growth model is able
617 to fit the data (as demonstrated in Ochsenbein et al. (2014)) is a consequence of G_w (or
618 the initial growth rate distribution) being a function of size, not the other way around.
619 Concerning the numerical complexity, the relatively high dimensionality of the *gap*
620 model together with the strongly varying convective terms make it barely suited for
621 use within an optimization routine. It is also for this reason that the achieved fits can
622 at best be described as a proof-of-concept. We thus do not recommend the use of such
623 models for the design or optimization of real processes, particularly given the unknown
624 physical nature of both w and G_w .

625 5.3. *Scientific and Industrial Relevance*

626 Regarding the scientific and industrial value of this work, first and foremost, we high-
627 light the fact that the current study is indeed one of seed crystals and their properties,
628 i.e., crystals which enter the process with a history. Studies of seed materials are highly
629 relevant, since the overwhelming majority of industrial processes carried out in batch
630 crystallizers are seeded; however little is known regarding the systematic and mecha-
631 nistically informed preparation of such particles.

632 Additionally, this work concerns itself with the evolution of GRD over time. As such, it
633 lays the basis for a better understanding of how growth kinetics are affected by process
634 conditions. Note that these effects might be either unintentional, as in the case of
635 needle breakage, or deliberate. Clearly, gaining insight in what causes GRD and how

636 to reproduce it-or even minimize it-could be of considerable value in this context.

637 **6. Conclusion and Outlook**

638 The growth rate dispersion of β L-glutamic acid needles in the length direction was
639 investigated by means of two independent imaging methods, one dedicated to the mea-
640 surement of the instantaneous particle size and shape distribution in the crystallizer
641 over time, the other to the tracking of the particle morphology for individual crystals.
642 After deducing the presence of a *growth affecting property (gap)* in the crystals from
643 single crystal data, the population balance framework was used to design a description
644 of the system, the *gap* model, that allows combining the complementary information
645 contained in both data sets through the initial condition. It was further shown that the
646 *gap* content in the particles is subject to change over time. Finally, through a proof-of-
647 concept fitting procedure, the hypothesis that the rate of change is influenced by particle
648 size was formulated and found to yield a plausible explanation for the experimentally
649 observed phenomena. However, in order to conclusively rule out other possibilities,
650 further experimental data would be required, as we have highlighted throughout this
651 article.

652 We perceive the value of this study to be two-fold: first, it highlights the added benefit
653 that results from using multi-scale approaches that employ a combination of indepen-
654 dent measurement techniques to the study of crystallization phenomena, since indi-
655 vidual tools may not offer full insight into the different aspects affecting the process.
656 While this work focuses on crystal growth, we believe this to be true also in the case
657 of nucleation, agglomeration, etc. Second, the present work showcases the potential
658 benefits of using quantitative analysis of experimental data sets through process mod-
659 els. While the resulting mathematical description may not necessarily be practical as
660 a design tool for process optimization, it represents a more comprehensive and physi-
661 cally sound view of the observed phenomena, thus allowing for a deeper understanding

662 of the process. The resulting qualitative lessons could then be used to guide process
663 development as well as to identify further research directions in order to establish a
664 more complete picture of crystallization.

665 **Acknowledgements**

666 The authors are thankful to the Swiss National Science Foundation for their support
667 (project number 200021-155971).

B	birth term in the PBE	$[\text{m}^{-2} \text{kg}^{-1} \text{s}^{-1}]$
C	space domain	$[-]$
c	solute concentration in the liquid phase	$[\text{kg kg}^{-1}]$
c_0	initial solute concentration in the liquid phase	$[\text{kg kg}^{-1}]$
c^*	solubility	$[\text{kg kg}^{-1}]$
c_{eff}^*	effective solubility	$[\text{kg kg}^{-1}]$
D	death term in the PBE	$[\text{m}^{-2} \text{kg}^{-1} \text{s}^{-1}]$
f	number density function	$[\text{m}^{-n} \text{kg}^{-1}]$
f_s	marginal shape distribution	$[\text{m}^{-n} \text{kg}^{-1}]$
f_0	PSD of seed crystals	$[\text{m}^{-n} \text{kg}^{-1}]$
\mathbf{G}	vector of rates of change	[varies]
$\hat{G}_1^{(i)}$	observed length growth rate of i 'th crystal in single crystal experiments	$[\text{m s}^{-1}]$
g	inverse of G_1 at given S and \mathbf{p}	$[-]$
\mathbf{k}	vector of growth rate parameters	[varies]
\mathbf{L}	vector of characteristic lengths	$[\text{m}]$
MRE_i	mean relative error of i 'th quantity	$[-]$
N_t	number of observations	$[-]$
N_v	number of measured outputs	$[-]$
P_w	<i>gap</i> -distribution	$[-]$
\mathbf{p}	vector of growth rate parameters	[varies]
R	gas constant	$[\text{J mol}^{-1} \text{K}^{-1}]$
S	supersaturation	$[-]$
S_0	peak supersaturation	$[-]$
T	temperature	$[\text{K}]$
t	time	$[\text{s}]$
V_c	single crystal volume	$[\text{m}^3]$
w	growth affecting property	$[-]$
$\hat{\mathbf{w}}$	<i>gap</i> dataset	$[-]$
w_s	molar strain energy	$[\text{J mol}^{-1}]$
\mathbf{x}	state vector of particle properties	[varies]
y_{ij}	output i at time j	[varies]
\mathbf{z}	state vector of continuous phase	[varies]

Greek letters

μ_{ij}	ij -cross moment of shape distribution	$[\text{m}^{i+j} \text{kg}^{-1}]$
ρ_c	crystal density	$[\text{kg m}^{-3}]$
σ_{11}	standard deviation of shape distribution in L_1 direction	$[\text{m}]$
Φ	objective function for parameter estimation	$[-]$

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Table 1: Overview of Growth Rate Dispersion Modeling Works. L refers to a characteristic size while w represents a GRD related property.

Reference	Internal PBE coordinates	Growth Rate	G_w	Remarks
This work	L_1, L_2, w	BCF or strain	non-zero	
Gerstlauer et al. (2001)	L, w	strain	non-zero	
Ma and Wang (2008)	L_1, L_2, L_3	strain	n/a	w not an independent property, but explicit function of \mathbf{L}
Bohlin and Rasmuson (1992)	L, w	BCF	zero	
Klug and Pigford (1989)	L, w	BCF	zero	
Zumstein and Rousseau (1987a,b)	L, w	BCF	zero	Combined CCG + RF model
Jones and Larson (2000)	n/a	BCF and Strain	n/a	
Shiau (2003)	n/a	BCF	n/a	

Table 2: Nonlinear regression results of G_1 data

	Estimate	st. dev.	t-statistic	p-value
k_1	3.00E-03	1.00E-03	2.41	0.02
k_2	0.04	0.06	0.61	0.54
k_3	0.32	0.07	4.38	3.00E-03

Table 3: Mean relative errors (MREs) of PSSD data for different fittings and predictions

Description	S_0 [-]	T [°C]	MRE_{conc} [%]	MRE_{length} [%]	MRE_{stddev} [%]
Static <i>gap</i> model fit	1.10	25	0.3	2.7	7.1
	1.15	25	0.2	20.9	0.7
	1.20	25	0.4	71.0	3.3
	1.25	25	1.5	71.5	1.4

Static <i>gap</i> model fit (additional fitting of measured G_1 data)	1.10	25	0.4	1.1	7.1
	1.15	25	0.5	1.7	1.4
	1.20	25	0.1	0.4	1.6
	1.25	25	0.6	0.2	1.4

Dynamic <i>gap</i> model fit	1.10	25	0.4	1.0	7.3
	1.15	25	0.5	0.5	4.3
	1.20	25	0.2	1.2	0.02
	1.25	25	0.01	1.0	2.3

Predict experiment with $S_0 = 1.15$, fit remaining	1.15	25	0.2	1.7	4.8
Predict experiment with $S_0 = 1.20$, fit remaining	1.20	25	0.04	2.4	1.6
Predict experiment at $T = 30^\circ\text{C}$ with fit at $T = 25^\circ\text{C}$	1.18	30	1.8	0.2	7.7

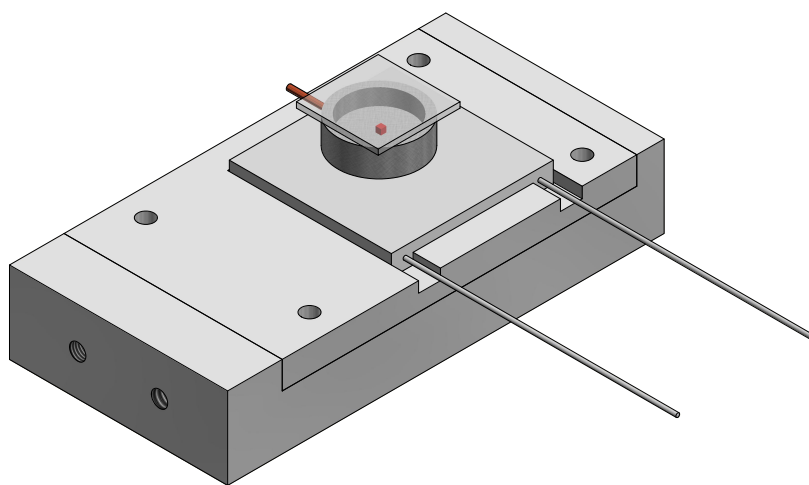


Figure 1: Schematic of the Hot Stage Setup.

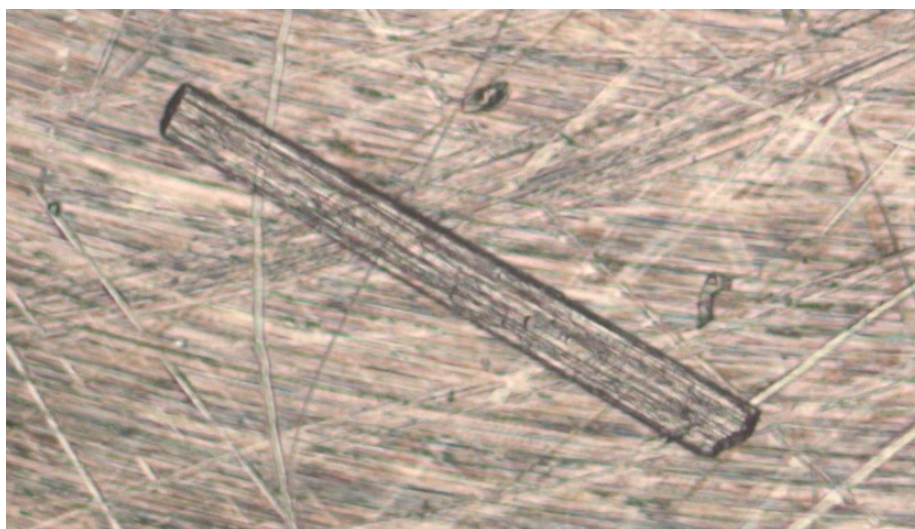


Figure 2: Example image of a β L-glutamic acid crystal in the hot stage.

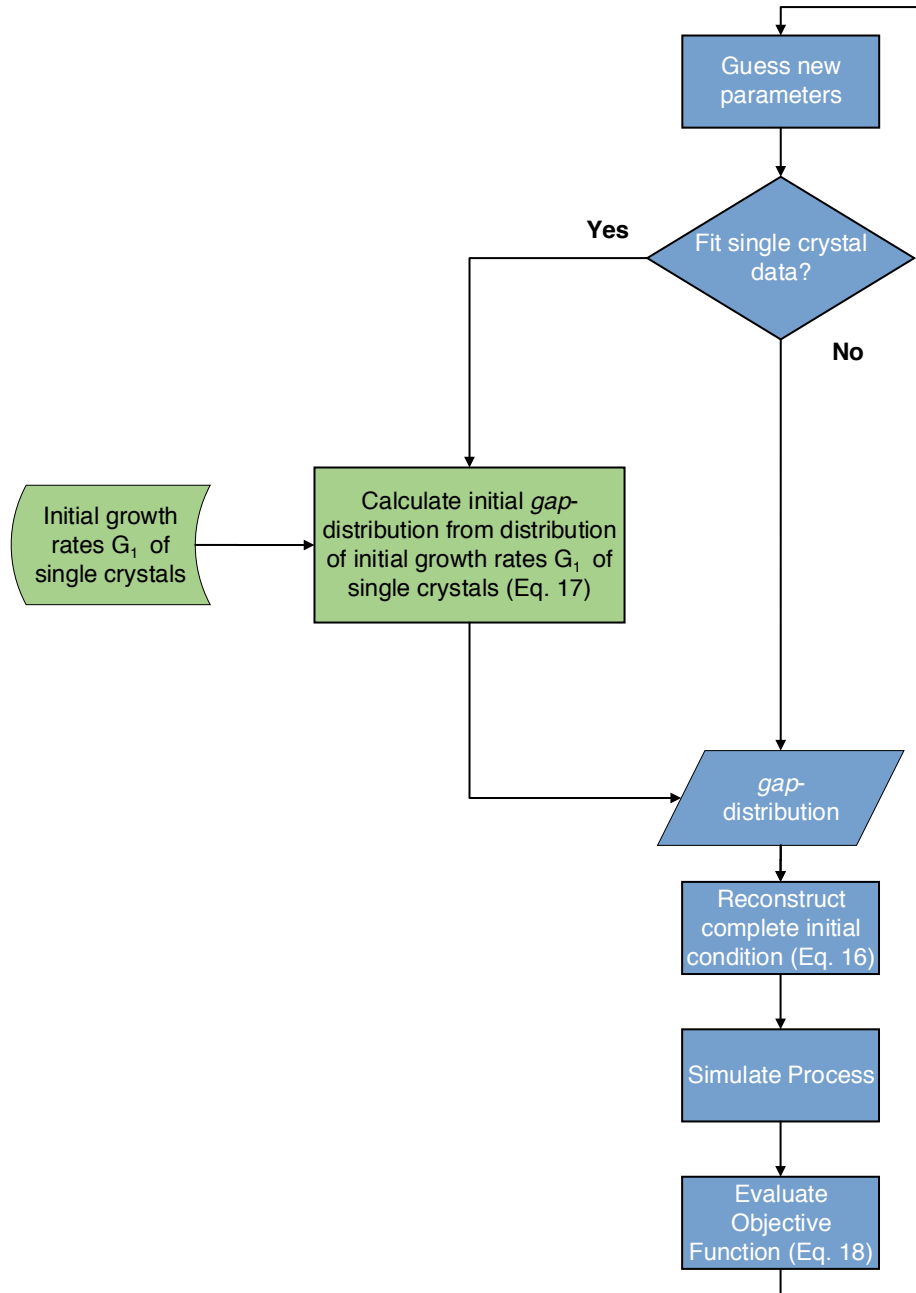


Figure 3: Schematic of the fitting procedure.

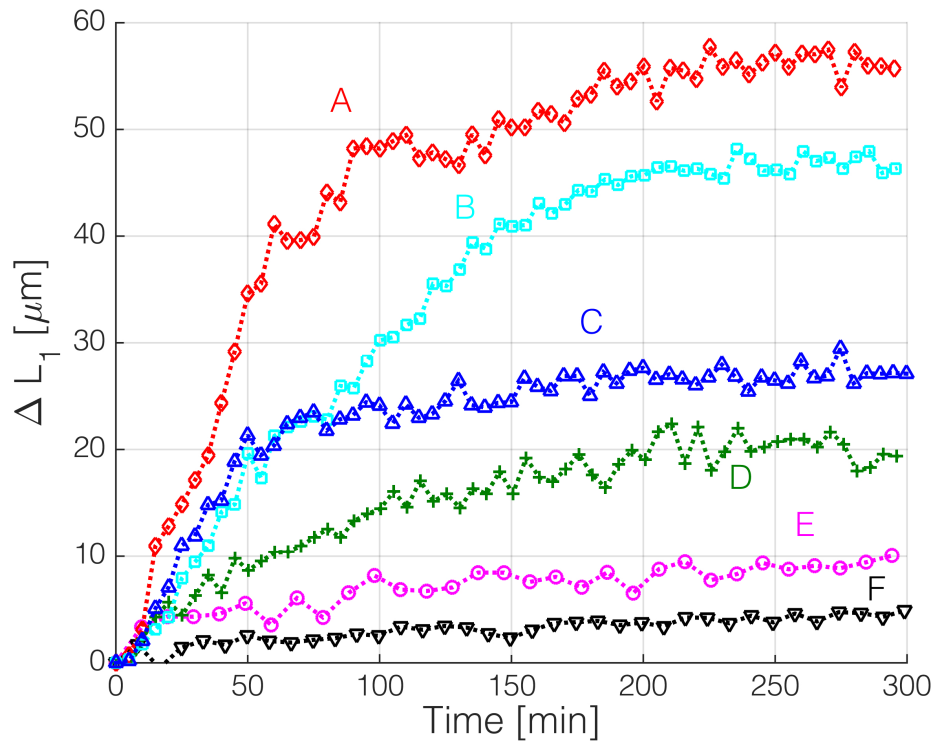


Figure 4: ΔL_1 vs. time curve for different crystals. Individual measurement points are given by the mean of three size evaluations. Initial size vectors for the crystals: $\mathbf{L}^A = [505, 59]^T \mu\text{m}$, $\mathbf{L}^B = [442, 38]^T \mu\text{m}$, $\mathbf{L}^C = [261, 46]^T \mu\text{m}$, $\mathbf{L}^D = [152, 45]^T \mu\text{m}$, $\mathbf{L}^E = [228, 34]^T \mu\text{m}$, $\mathbf{L}^F = [177, 33]^T \mu\text{m}$.

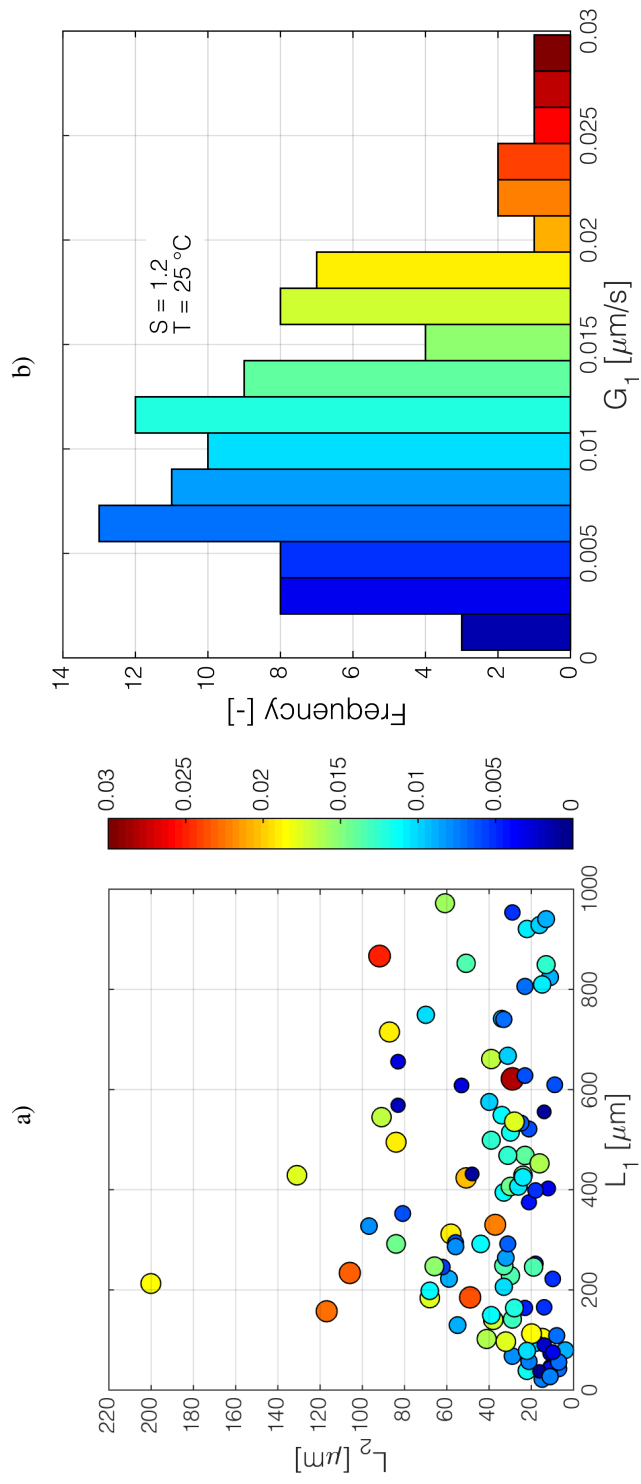


Figure 5: (a) Scatter plot of growth rates G_1 as function of initial crystal size and (b) histogram of growth rates. Size and color of markers in (a) indicate the magnitude of the growth rate.

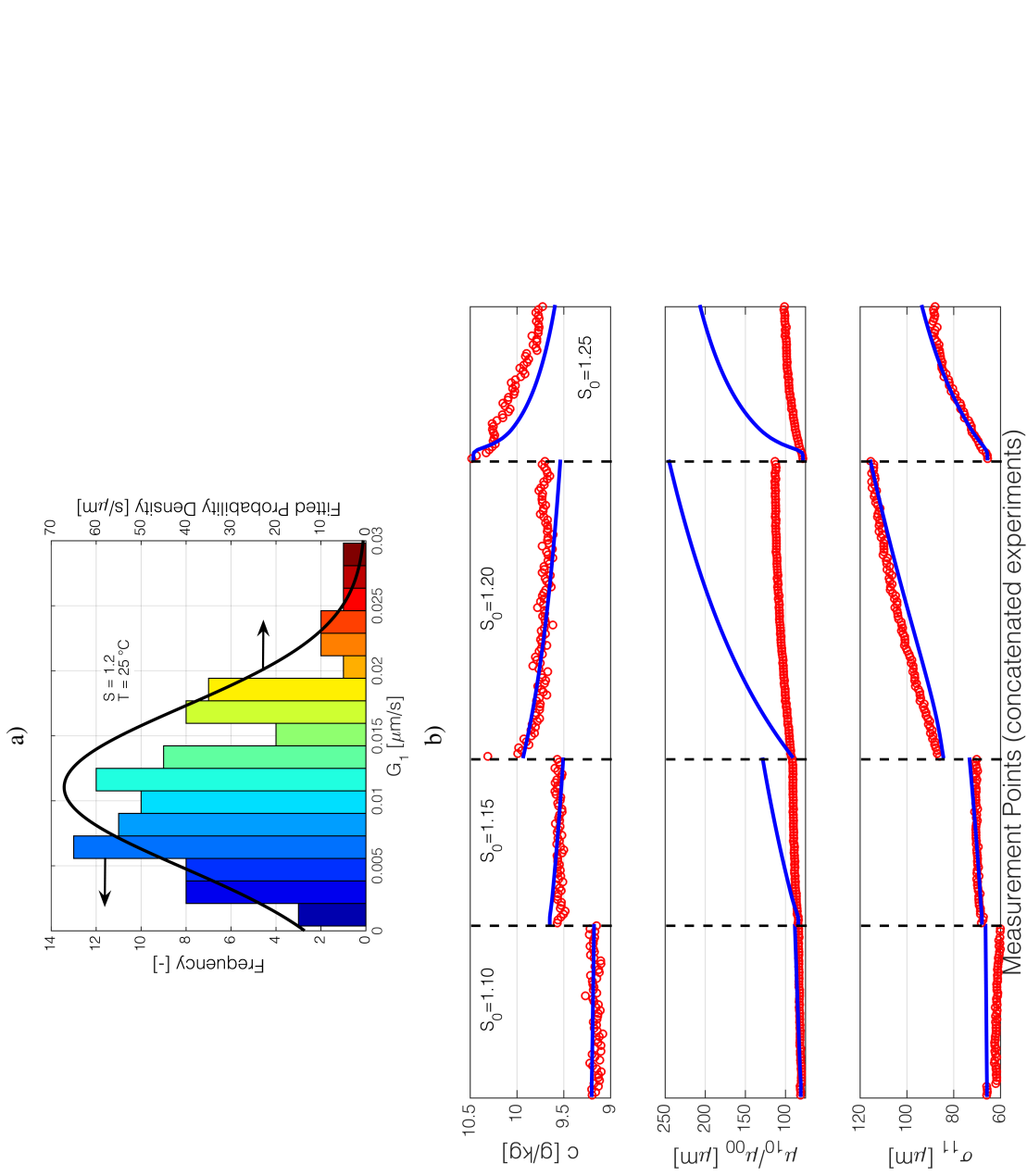


Figure 6: Results of the static *gap* model with no additional degrees of freedom. a) Comparison between measured (single crystal experiments) and fitted growth rate distribution; b) fit result for batch desupersaturation experiments conducted at the same final temperature (concatenated outputs).

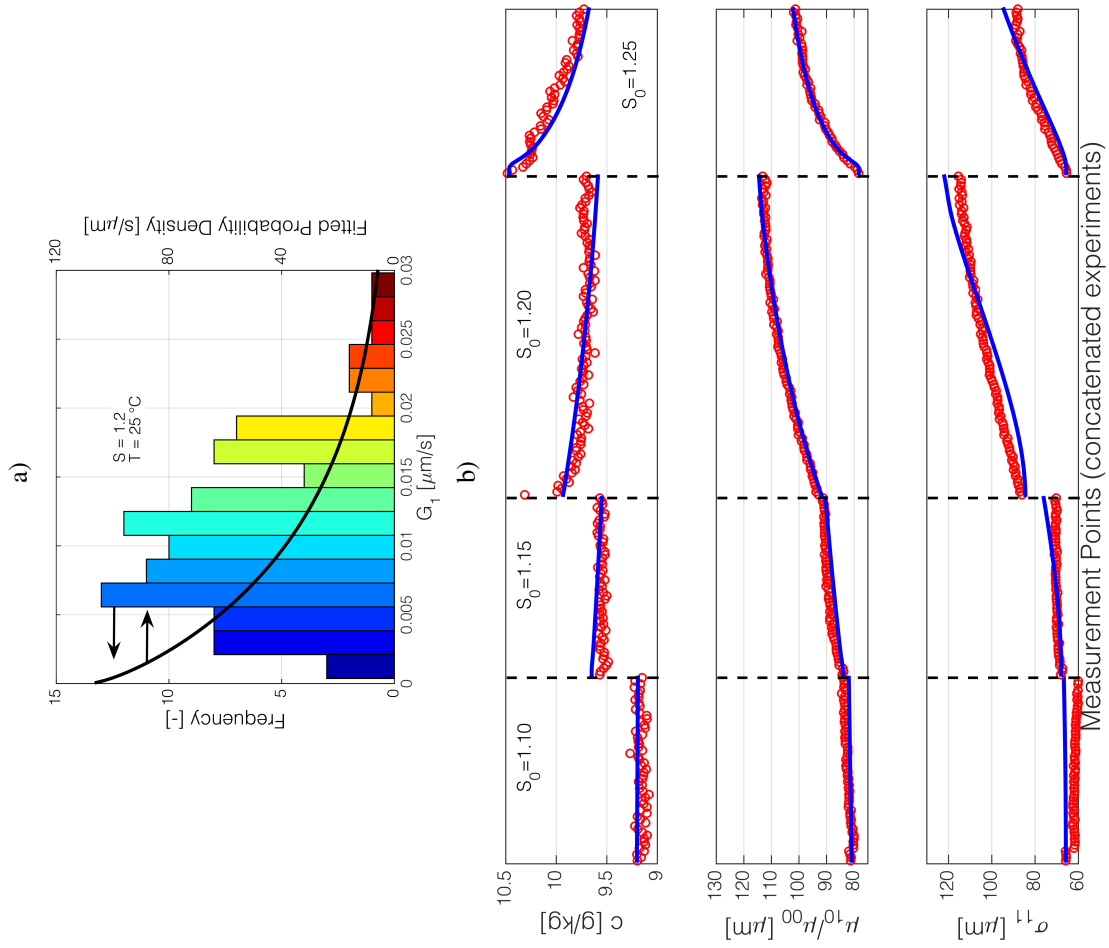


Figure 7: Results of the static *gap* model with parameterized *gap* distribution. a) Comparison between measured (single crystal experiments) and fitted growth rate distribution; b) fit result for batch desupersaturation experiments conducted at the same final temperature (concatenated outputs).

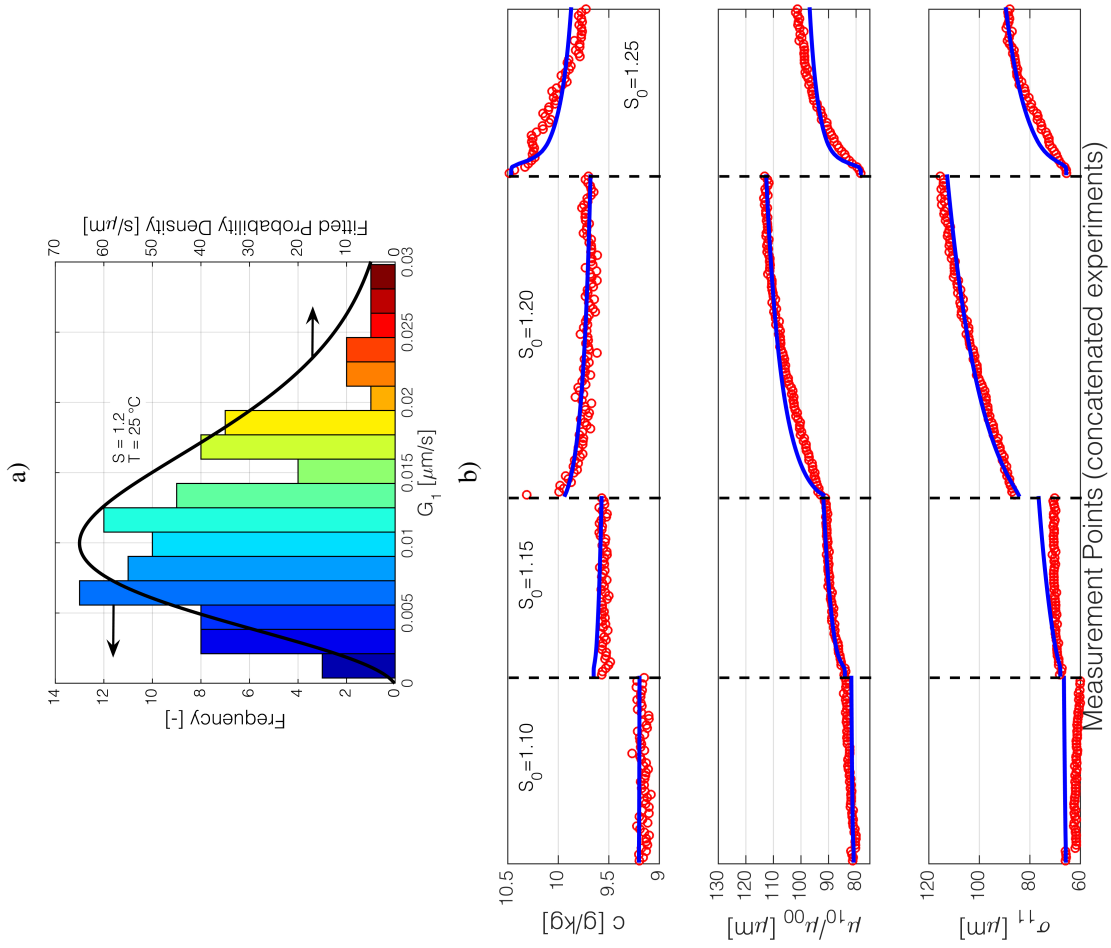


Figure 8: Results of the dynamic *gap* model with no additional degrees of freedom. a) Comparison between measured (single crystal experiments) and fitted growth rate distribution; b) fit result for batch desupersaturation experiments conducted at the same final temperature (concatenated outputs).

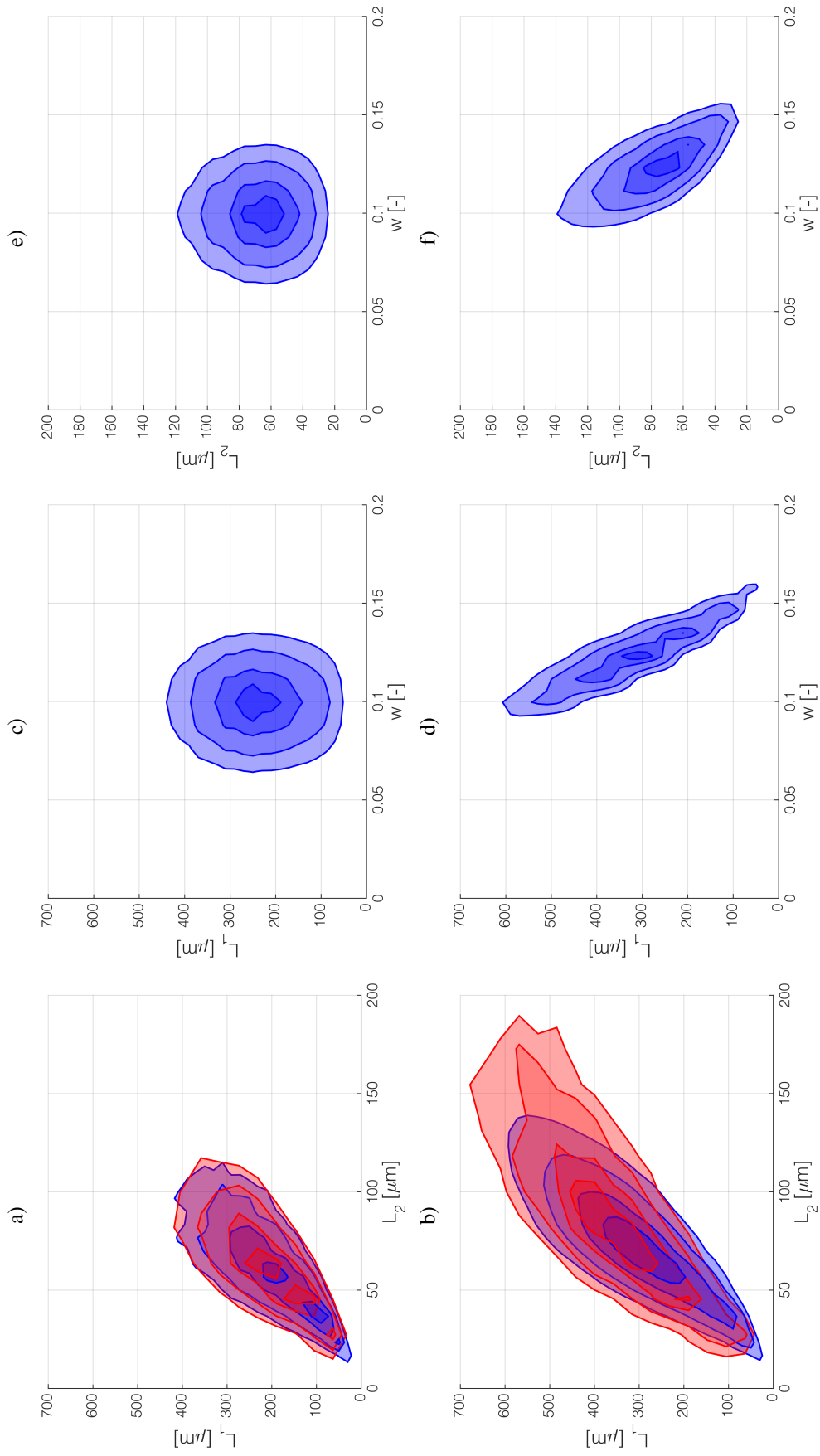


Figure 9: Volume weighted marginal distributions of fitted experiment with $S_0 = 1.20$. a)+b) Initial and final PSSD. Blue contour lines indicate model results while red lines indicate the experimental data; c)+d) Initial and final distributions (projection on L_1 vs. w plane);e)+f) Initial and final distributions (projection on L_2 vs. w plane). All contour lines are drawn at 30%, 50%, 75% and 90% of the respective maximum.

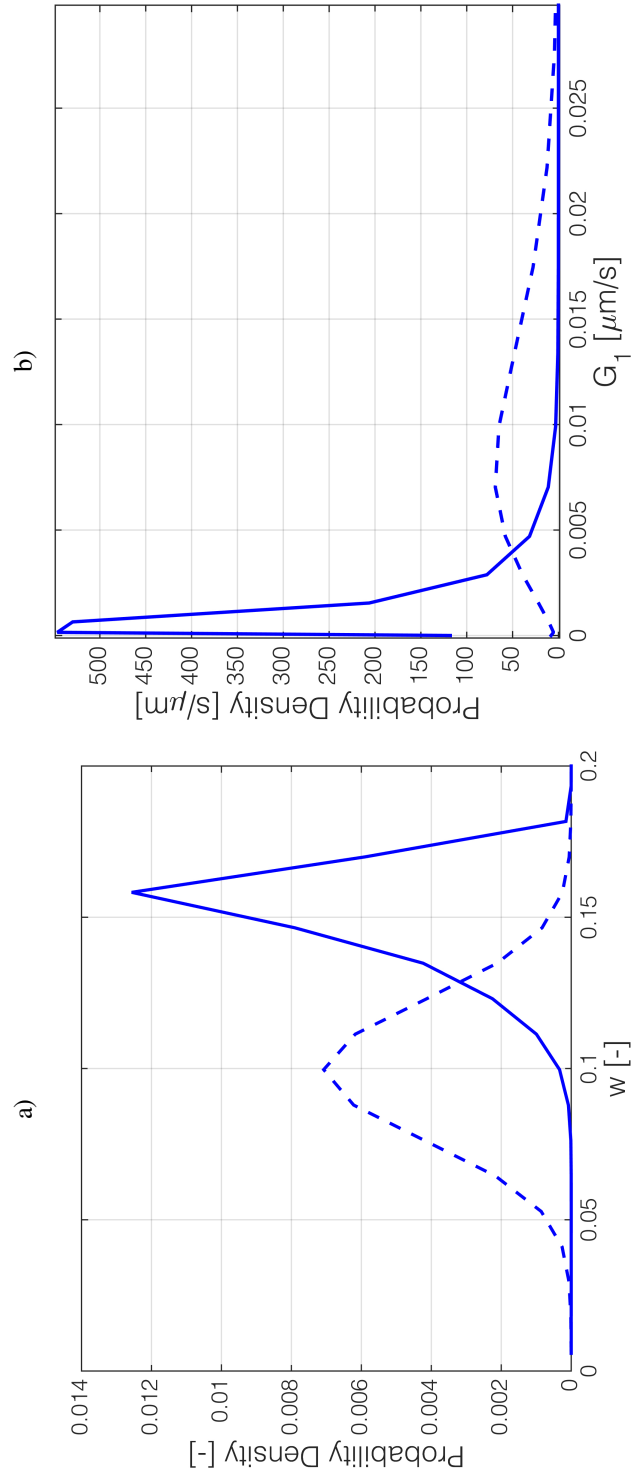


Figure 10: Comparison of the initial (dashed) and final (solid) gap and G_1 distribution for the experiment with $S_0 = 1,20$ in the model. a) gap distribution; b) growth rate distribution.